

Part 70 Operating Permit Amendment

Permit Amendment No.: **2631-245-0006-V-01-2** Effective Date:

Facility Name: **International Paper – Augusta Mill**
4278 Mike Padgett Highway (Highway 56 South)
Augusta, Georgia 30906 (Richmond County)

Mailing Address: P.O. Box 1425
Augusta, Georgia 30903-1425

Parent/Holding Company: International Paper

Facility AIRS Number: 04-13-245-00006

In accordance with the provisions of the Georgia Air Quality Act, O.C.G.A. Section 12-9-1, et seq and the Georgia Rules for Air Quality Control, Chapter 391-3-1, adopted pursuant to and in effect under the Act, the Permittee described above is issued a construction permit for:

Modification to the existing chip bin and chip meter on the No. 3 Digester, which increases the facility-wide production. Also the modification of the Paper Machines to reduce the number of paper breaks.

This Permit Amendment shall also serve as a final amendment to the Part 70 Permit unless objected to by the U.S. EPA or withdrawn by the Division. The Division will issue a letter when this Operating Permit amendment is finalized.

This Permit Amendment is conditioned upon compliance with all provisions of The Georgia Air Quality Act, O.C.G.A. Section 12-9-1, et seq, the Rules, Chapter 391-3-1, adopted and in effect under that Act, or any other condition of this Permit Amendment and Permit No. 2631-245-0006-V-01-0. Unless modified or revoked, this Permit Amendment expires upon issuance of the next Part 70 Permit for this source.

This Permit Amendment may be subject to revocation, suspension, modification or amendment by the Director for cause including evidence of noncompliance with any of the above; or for any misrepresentation made in Application No. 14747 dated September 25, 2003; any other applications upon which this Permit Amendment or Permit No. 2631-245-0006-V-01-0 are based; supporting data entered therein or attached thereto; or any subsequent submittal or supporting data; or for any alterations affecting the emissions from this source.

This Permit Amendment is further subject to and conditioned upon the terms, conditions, limitations, standards, or schedules contained in or specified on the attached **18** pages, which pages are a part of this Permit Amendment, and which hereby become part of Permit No. 2631-245-0006-V-01-0.

Director
Environmental Protection Division

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PART 1.0 FACILITY DESCRIPTION

1.3 Process Description of Modification

The International Paper-Augusta Mill is modifying the No. 3 Digester System, in particular the chip bin, chip meter, and pumps, to improve pulp production capacity. This modification enhances the mill-wide pulp production efficiency by assuring that the most efficient digester is the primary digester. The potential facility-wide production increases due to this modification; thus all mill operations potentially will see an increase in production rate and emissions.

Also during this modification, the Paper Machines are improved with systems to reduce the number of paper breaks. These improvements include installing suction pickups for the No. 3 Paper Machine, to help guide the paper from the fourdrinier section to the press section. A reduction in paper breaks translates into a reduction in downtime, rejected product, and allows a potential increase in annual finished tons of paper produced. To restrict the emissions potential and at the request of the facility, a facility-wide production limit is included in this amendment. Thus, paper machine production will now be effectively bottlenecked and the paper machine emissions are effectively capped.

PART 2.0 REQUIREMENTS PERTAINING TO THE ENTIRE FACILITY

2.1 Facility Wide Emission Caps and Operating Limits

- 2.1.1 The Permittee shall not produce more than 1,894 oven-dried tons of unbleached pulp per day from the entire facility based on a twelve-month rolling average.
[40 CFR 52.21]

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PART 3.0 REQUIREMENTS FOR EMISSION UNITS

Note: Except where an applicable requirement specifically states otherwise, the averaging times of any of the Emissions Limitations or Standards included in this permit are tied to or based on the run time(s) specified for the applicable reference test method(s) or procedures required for demonstrating compliance.

3.1.1 Additional Emission Units

Emission Units		Specific Limitations/Requirements		Air Pollution Control Devices	
ID No.	Description	Applicable Requirements/Standards	Corresponding Permit Conditions	ID No.	Description
LK1A	No. 1 Lime Kiln	40 CFR 63 Subpart MM	3.3.35, 4.2.13, 6.2.1, 6.2.29, 6.2.30, 6.2.32	LK1B LK1C	No. 1 Kiln Venturi Scrubber and No. 1 Kiln Cyclone
LK2A	No. 2 Lime Kiln	40 CFR 52.21 40 CFR 63 Subpart MM	3.3.1, 3.3.12, 4.2.13, 6.2.1, 6.2.29, 6.2.30, 6.2.32	LK2B LK2C	No. 2 Kiln Venturi Scrubber and No. 2 Kiln Dust Bin (cyclone)
RB2A	No. 2 Recovery Boiler	40 CFR 52.21 40 CFR 63 Subpart MM	3.2.4, 3.3.36, 4.2.13, 6.2.4, 6.2.25, 6.2.26, 6.2.27, 6.2.29, 6.2.30, 6.2.32	RB2B BLOX	No. 2 Recovery Precipitator and Black Liquor Oxidation System
RB3A	No. 3 Recovery Boiler	40 CFR 63 Subpart BB 40 CFR 63 Subpart MM	3.3.2, 4.2.13, 6.2.4, 6.2.29, 6.2.30, 6.2.32	RB3B	No. 3 Recovery Precipitator
ST2A	No. 2 Smelt Tank	40 CFR 52.21 40 CFR 63 Subpart MM	3.3.37, 4.2.13, 5.2.2, 6.2.29, 6.2.30, 6.2.32	ST2B	No. 2 Smelt Wet Scrubber
ST3A	No. 3 Smelt Tank	40 CFR 63 Subpart MM	3.3.5, 4.2.13, 5.2.2, 6.2.29, 6.2.30, 6.2.32	ST3B	No. 3 Smelt Wet Scrubber
NCGB	Nos. 2 and 3 Digesters; No. 3 Evaporator System	40 CFR 60 Subpart BB, 391-3-1-.02(2)(gg)	3.3.12	LK2A PB1A PB2A	No. 2 Lime Kiln No. 1 Power Boiler No. 2 Power Boiler
NCGC	No. 1 Digester; Nos. 1 and 2 Evaporator Systems; No. 1 Low Pressure Feeder; No. 2 Evaporator Hotwell	391-3-1-.02(2)(gg)	3.3.12	LK2A PB1A PB2A	No. 2 Lime Kiln No. 1 Power Boiler No. 2 Power Boiler
NCGD	Dilute TRS Gases from No. 2 and 3 Digester chip bins; Nos. 1, 2, and 3 Digester Blow Tanks; and the black liquor oxidation vent.	40 CFR 52.21	None	LK2A PB1A PB2A	No. 2 Lime Kiln No. 1 Power Boiler No. 2 Power Boiler
NCGE	Concentrated TRS Gases from NCGA, NCGB, and NCGC	40 CFR 52.21	3.2.5, 3.3.12, 4.2.11, 5.2.2, 6.2.28	LK2A PB1A PB2A WLSA WLSB	No. 2 Lime Kiln No. 1 Power Boiler No. 2 Power Boiler White Liquor Scrubber White Liquor Scrubber

* Generally applicable requirements contained in this permit may also apply to emission units listed above.

3.2 Equipment Emission Caps and Operating Limits

3.2.4 The Permittee shall not emit more than 623 tons per year of SO₂ emissions from the No. 2 Recovery Boiler (RB2A), based on a twelve-month rolling total.
[40 CFR 52.21 Avoidance]

- 3.2.5 The Permittee shall operate the White Liquor Scrubbers (WLSA and WLSB) with a minimum removal efficiency of 65 percent (by weight) for total reduced sulfur compounds. [40 CFR 52.21. Avoidance]

3.3 Equipment Federal Rule Standards

No. 2 Lime Kiln

- 3.3.1 The Permittee shall not discharge or cause the discharge into the atmosphere from No. 2 Lime Kiln any gases which:
- b. Contain particulate matter emissions in excess of 0.064 grains/dscf at 10 percent oxygen). [40 CFR 52.21, 40 CFR 63.862(a)(ii)(A), 40 CFR 60.282(a)(3)(i) (subsumed), and 40 CFR 60.282(a)(3)(ii) (subsumed)]
 - c. Deleted.

No. 3 Recovery Boiler

- 3.3.2 The Permittee shall not discharge or cause the discharge into the atmosphere from No. 3 Recovery Boiler RB3A any gases which:
- b. Contain particulate matter emissions in excess of 0.021 grains/dscf corrected to 8% oxygen. [40 CFR 63.862(a)(ii)(A) and 40 CFR Subpart BB (subsumed)]

No. 3 Smelt Tank

- 3.3.5 The Permittee shall not discharge or cause the discharge into the atmosphere from the No. 3 Smelt Tank any gases which contain particulate matter emissions in excess of 0.20 pound per ton of black liquor solids (dry weight). [40 CFR 60 Subpart BB and 40 CFR 63.862(a)(ii)(A)]

Pulping Process LVHC NCG Systems

- 3.3.12 The Permittee shall process the NCG System gases in the following manner:
- a. When combusting TRS gases from NCGB and NCGC, the gases shall be introduced into the flame zone of Nos. 1 and 2 Power Boilers. [40 CFR 60 Subpart BB and 391-3-1-.03(2)(gg)]

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- b. When combusting the concentrated TRS gas streams of Emission Group NCGE in Nos. 1 and 2 Power Boilers, the gases shall be scrubbed in one of the White Liquor Scrubbers (WLSA and WLSB) prior to entering the boilers. The White Liquor Scrubbers (WLSA and WLSB) operate in parallel and act as backups to each other. In the event of malfunction of the scrubber and the unavailability of Lime Kiln No. 2 as the primary incineration device, the Permittee shall be subject to the reporting requirements of 6.1.2.
[40 CFR 52.21 Avoidance]

No. 1 Lime Kiln

- 3.3.35 The Permittee shall not discharge or cause the discharge into the atmosphere from No. 1 Lime Kiln LK1A any gases that contain particulate matter emissions in excess of 0.176 grains/dscf at 10% percent oxygen.
[40 CFR 63.862(a)(ii)(A)]

No. 2 Recovery Boiler

- 3.3.36 The Permittee shall not discharge or cause the discharge into the atmosphere from the No. 2 Recovery Boiler (RB2A) any gases which contain particulate matter in excess of 0.055 grains/dscf at 8% oxygen.
[40 CFR 52.21 and 40 CFR 63.862(a)(ii)(A)]

No. 2 Smelt Tank

- 3.3.37 The Permittee shall not discharge or cause the discharge into the atmosphere from the No. 2 Smelt Tank (ST2A) any gases that contain particulate matter emissions in excess of 0.585 pound per ton of black liquor solids.
[40 CFR 52.21 and 40 CFR 63.862(a)(ii)(A)]

PART 4.0 REQUIREMENTS FOR TESTING**4.1 General Testing Requirements**

4.1.3 Performance and compliance tests shall be conducted and data reduced in accordance with applicable procedures and methods specified in the Division's Procedures for Testing and Monitoring Sources of Air Pollutants. The methods for the determination of compliance with emission limits listed under Sections 3.2, 3.3, 3.4 and 3.5 are as follows:

- a. Methods 1 and 1A for selection of sampling port location and number of traverse points.
[40 CFR 63.865(b)(5)(i)]
- b. Method 2, 2A, 2C, 2D, 2F, or 2G for determining stack gas velocity and volumetric flow rate
[40 CFR 63.865(b)(5)(ii)]
- c. Method 3, 3A, or 3B for determining the oxygen concentration. The gas sample must be taken at the same time and at the same traverse points as the particulate sample. The voluntary consensus standard ANSI/ASME PTC 19.10-1981 – Part 10 may be used as an alternative to Method 3B.
[40 CFR 63.865(b)(3) and 40 CFR 63.865(b)(5)(iii)]
- d. Method 4 for determining moisture content of stack gas.
[40 CFR 63.865(b)(5)(iv)]
- e. Method 5 or 29 for determining the concentration or mass of particulate matter emitted. Method 17 may be used in lieu of Method 5 or Method 29 if a constant value of 0.009 g/dscm (0.004 gr/dscf) is added to the results of Method 17, and the stack temperature is no greater than 205°C (400°F). For Methods 5, 29, and 17, the sampling time and sample volume for each run must be at least 60 minutes and 0.90 dscm (31.8 dscf) and water must be used as the cleanup solvent instead of acetone in the sample recovery procedure.
[40 CFR 63.865(b)(1)]
- t. For Nos. 2 and 3 Recovery Boilers and Nos. 1 and 2 Lime Kilns, the particulate matter concentration must be corrected to the appropriate oxygen concentration using the procedures of 40 CFR 63.865(b)(2).
[40 CFR 63.865(b)(2)]

Minor changes in methodology may be specified or approved by the Director or his designee when necessitated by process variables, changes in facility design, or improvement or corrections that, in his opinion, render those methods or procedures, or portions thereof, more reliable.

[391-3-1-.02(3)(a)]

4.2 Specific Testing Requirements

- 4.2.11 The Permittee shall conduct an initial performance test on White Liquor Scrubbers WLSA and WLSB each within 60 days of achieving maximum production but no later than 365 days after completion of construction to determine compliance with Condition 3.2.5 using the test methods and procedures listed in Condition 4.1.3.
[40 CFR 52.21 Avoidance]

- 4.2.12 During the initial performance test required in Condition 4.2.11, the Permittee must establish the appropriate operating ranges for the monitoring parameters in Conditions 5.2.2.g and 5.2.2.h. Alternately, the Permittee may base the operating ranges on values recorded during previous performance tests or conduct additional performance tests for the specific purposes of establishing operating ranges, provided that the test data used to establish the operating ranges are obtained, or have been obtained, using the test methods required by Condition 4.1.3.
[40 CFR 63.7, 391-3-1-.02(3) and 391-3-1-.03(2)(c)]

- 4.2.13 If an initial performance test has not yet been performed for Nos. 2 and 3 Recovery Furnaces, Nos. 2 and 3 Smelt Dissolving Tanks, and Nos. 1 and 2 Lime Kilns, the Permittee shall conduct an initial performance test to determine compliance with Conditions 3.3.1, 3.3.2, 3.3.5, 3.3.35, 3.3.36, and 3.3.37 using the test methods and procedures listed in Condition 4.1.3. This initial performance test shall be conducted before November 9, 2004.
[40 CFR 63.865]

- 4.2.14 During the initial performance test required in Condition 4.2.13, the Permittee must establish appropriate operating ranges for the monitoring parameters in Conditions 5.2.2.a, 5.2.2.b, and 5.2.2.c. Alternatively, the Permittee may base operating ranges on values recorded during previous performance tests or conduct additional performance tests for the specific purpose of establishing operating ranges, provided that test data used to establish the operating ranges are obtained, or have been obtained using the test methods required by Condition 4.1.3.
[40 CFR 63.864(j)(1) and 63.864(j)(2)]

PART 5.0 REQUIREMENTS FOR MONITORING (Related to Data Collection)

5.1 General Monitoring Requirements

- 5.1.1 Any continuous monitoring system required by the Division and installed by the Permittee shall be in continuous operation and data recorded during all periods of operation of the affected facility except for continuous monitoring system breakdowns and repairs. Monitoring system response, relating only to calibration checks and zero and span adjustments, shall be measured and recorded during such periods. Maintenance or repair shall be conducted in the most expedient manner to minimize the period during which the system is out of service.
[391-3-1-.02(6)(b)1]

5.2 Specific Monitoring Requirements

- 5.2.2 The Permittee shall install, calibrate, maintain, and operate a system to continuously monitor and record the indicated parameters on the following equipment. Where such performance specification(s) exist, each system shall meet the applicable performance specification(s) of the Division's monitoring requirements.
[391-3-1-.02(6)(b)1, 40 CFR 70.6(a)(3)(i), 40 CFR 63 Subpart MM and 40 CFR 52.21]
- c. Scrubbant flow rate and fan motor current for the Nos. 2 and 3 Smelt Dissolving Tank scrubbers ST2B and ST3B.
 - g. Pressure drop and scrubbant flowrate on the White Liquor Scrubber (WLSA).
 - h. Pressure drop and scrubbant flowrate on the White Liquor Scrubber (WLSB).

PART 6.0 OTHER RECORD KEEPING AND REPORTING REQUIREMENTS**6.1 General Record Keeping and Reporting Requirements**

6.1.7 For the purpose of reporting excess emissions, exceedances or excursions in the report required in Condition 6.1.4, the following excess emissions, exceedances, and excursions shall be reported:

[391-3-1-.02(6)(b)1 and 40 CFR 70.6(a)(3)(i)]

- b. Exceedances: (means for the purpose of this Condition and Condition 6.1.4, any condition that is detected by monitoring or record keeping that provides data in terms of an emission limitation or standard and that indicates that emissions (or opacity) do not meet the applicable emission limitation or standard consistent with the averaging period specified for averaging the results of the monitoring)
- x. Any single day during which the facility-wide pulping production exceeds 1,894 ODTUBP/day based on a twelve-month rolling average.
[40 CFR 52.21]
- xi. Any twelve consecutive month total SO₂ emissions from the No. 2 Recovery Boiler (Source Code: RB2A) that exceeds 623 tons.
[40 CFR 52.21]

40 CFR 63 Subpart MM

Periods of monitoring exceedances reported for Conditions 6.1.7.b.xii and xiii shall be a violation of 40 CFR 63 Subpart MM if the total period of monitoring exceedance (excluding periods of startup, shutdown, or malfunction) divided by the total process operating time, in a quarterly reporting period, exceeds 6%.
[40 CFR 63.864(k)(2)(i)]

- xii. No. 2 Recovery Boiler for opacity greater than 35% (six-minute average).
- xiii. No. 3 Recovery Boiler for opacity greater than 35% (six-minute average).

Periods of monitoring exceedances reported for 6.1.7.b.xiv through xxi shall be a violation of 40 CFR 63 Subpart MM when six or more 3-hour average parameter values (excluding periods of startup, shutdown, or malfunction) within any 6-month reporting period are outside than the parameter limits listed below. For purposes of determining the number of non-opacity monitoring exceedances, no more than one exceedance will be attributed in any given 24-hour period.
[40 CFR 63.864(k)(2)(i) and (iii)]

- xiv. No. 1 Lime Kiln Scrubber differential pressure less than 7.5 inches of water while firing natural gas or 11.9 inches of water while firing fuel oil.
- xv. No. 1 Lime Kiln Scrubber flow less than 300 gpm.

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- xvi. No. 2 Lime Kiln Scrubber differential pressure less than 23.4 inches of water.
 - xvii. No. 2 Lime Kiln Scrubber flow less than 540 gpm.
 - xviii. No. 2 Smelt Tank Scrubber flow less than 150 gpm.
 - xix. No. 2 Smelt Tank Scrubber fan motor amperage reading less than 77 amps.
 - xx. No. 3 Smelt Tank Scrubber flow less than 340 gpm.
 - xxi. No. 3 Smelt Tank Scrubber fan motor amperage reading less than 68 amps.
- c. Excursions: (means for the purpose of this Condition and Condition 6.1.4, any departure from an indicator range or value established for monitoring consistent with any averaging period specified for averaging the results of the monitoring)

Lime Kilns

- i. Any three hour period during which the average pressure drop or scrubbant flow rate for either lime kiln scrubber falls below the following values:
 - A. No. 1 Lime Kiln Scrubber LK1B: 7.5 inches of water while firing natural gas, 11.9 inches water while firing fuel oil, or 300 gpm.
 - B. No. 2 Lime Kiln Scrubber LK2B: 23.4 inches of water or 540 gpm.

White Liquor Scrubbers

- xxi. Any 3-hour period during which the average pressure drop or scrubbant liquor flow rate, for the White Liquor Scrubber WLSA, measured in accordance with Condition 5.2.2.g, falls outside the submitted and Division-approved operating ranges set as required by Condition 4.2.12.
[40 CFR 52.21]
 - xxii. Any 3-hour period during which the average pressure drop or scrubbant liquor flow rate, for the White Liquor Scrubber WLSB, measured in accordance with Condition 5.2.2.h, falls outside the submitted and Division-approved operating ranges set as required by Condition 4.2.12.
[40 CFR 52.21]
- d. In addition to the excess emissions, exceedances and excursions specified above, the following should also be included with the report required in Condition 6.1.4:
- xi. Any period when ten consecutive 6-minute opacity averages result in a measurement greater than 20% opacity for the No. 2 Recovery Boiler.
[40 CFR 63.864(k)(i)]

- xii. Any period when ten consecutive 6-minute opacity averages result in a measurement greater than 20% opacity for the No. 3 Recovery Boiler.
[40 CFR 63.864(k)(i)]

6.2 Specific Record Keeping and Reporting Requirements

Lime Kilns

- 6.2.1 The Permittee shall maintain the daily records of the lime production rate in tons per day, mud flow, mud density, and percent solids for the Nos. 1 and 2 Lime Kilns.
[40 CFR 866(c)(2) and 391-3-1-.02(2)(b)1]

Recovery Boilers

- 6.2.4 The Permittee shall maintain the daily records of the black liquor solids firing rate and percent black liquor solids for the Nos. 2 and 3 Recovery Boilers.
[40 CFR 866(c)(1) and 391-3-1-.02(2)(b)1]

No. 3 Digester PSD Project

- 6.2.23 The Permittee shall keep daily records of the production of oven dried tons of unbleached pulp per day (ODTUBP/day) for the entire facility. The records shall be available for inspection or submittal to the Division upon request.
[391-3-1-.02(6)(b)1 and 40 CFR 70.6(a)(3)(i)]
- 6.2.24 The Permittee shall use the records required by Condition 6.2.23 to calculate the twelve-month rolling production average for the entire facility. These records shall be available for inspection or submittal to the Division upon request.
[391-3-1-.02(6)(b)1 and 40 CFR 70.6(a)(3)(i)]
- 6.2.25 The Permittee shall keep daily records of the fuel oil usage, in gallons, for the No. 2 Recovery Boiler (RB2A). The records shall be available for inspection or submittal to the Division upon request.
[391-3-1-.02(6)(b)1 and 40 CFR 70.6(a)(3)(i)]
- 6.2.26 The Permittee shall calculate, record, and maintain the calendar month sulfur dioxide emissions from the No. 2 Recovery Boiler. The emissions shall be calculated on a pounds per day basis using the emission factor of 2.3 lb of SO₂ emitted per ton of black liquor solids, the monthly fuel sulfur content as calculated using the fuel certifications required by Condition 6.2.9 or 6.2.10, the fuel oil usage records required by Condition 6.2.24, and the black liquor solids firing rate required by Condition 6.2.4. The collected information shall be used in the following equation to determine the calendar month SO₂ emissions:
[391-3-1-.02(6)(b)1 and 40 CFR 70.6(a)(3)(i)]

$$\left[\left(\frac{157 \cdot S(\% \text{ sulfur}) \text{ lb } SO_2}{1000 \text{ gal}} \cdot \frac{\text{Fuel usage}}{\text{month}} \right) + \left(\frac{2.3 \text{ lb } SO_2}{\text{ton BLS}} \cdot \frac{\text{BLS usage}}{\text{month}} \right) \right] \cdot \frac{1 \text{ ton}}{2000 \text{ lb}} = \frac{\text{ton } SO_2}{\text{month}}$$

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- 6.2.27 The Permittee shall calculate, record, and maintain the twelve-month rolling total sulfur dioxide emissions from the No. 2 Recovery Boiler using the calculated monthly sulfur dioxide emissions from Condition 6.2.26.
[391-3-1-.02(6)(b)1 and 40 CFR 70.6(a)(3)(i)]
- 6.2.28 The operating ranges for the monitoring parameters in Conditions 5.2.2.g and 5.2.2.h determined using data collected during the performance test as per Condition 4.2.11, for the White Liquor Scrubbers (Source Codes WLSA and WLSB), must be submitted to the Division for approval within 60 days of the initial performance test. In the submittal, the Permittee must certify that no control techniques and processes have been modified subsequent to the testing upon which the data used to establish the operating parameter ranges were obtained.
[391-3-1-.02(6)(b)1 and 40 CFR 70.6(a)(3)(i)]

40 CFR 63 Subpart MM

- 6.2.29 The operating ranges for the monitoring parameters in Conditions 5.2.2.a, 5.2.2.b, and 5.2.2.c determined using data collected during the initial performance test as per Conditions 4.2.13 must be submitted to the Division for approval within 60 days of the initial performance test, unless the alternative approach presented in Condition 4.2.14 is selected by the Permittee. In the submittal, the Permittee must certify that no control techniques and processes have been modified subsequent to the testing upon which the data used to establish the operating parameter ranges were obtained.
[391-3-1-.02(6)(b)1 and 40 CFR 70.6(a)(3)(i)]
- 6.2.30 The Permittee shall notify the Division prior to any of the following:
- a. The air pollution control system is modified or replaced for the following process units: Nos. 2 and 3 Recovery Furnaces, Nos. 2 and 3 Smelt Dissolving Tanks, and Nos. 1 and 2 Lime Kilns.
[40 CFR 63.867(b)(3)(i)]
 - b. Any of the following units being shutdown for more than 60 consecutive days: Nos. 2 and 3 Recovery Furnaces, Nos. 2 and 3 Smelt Dissolving Tanks, and Nos. 1 and 2 Lime Kilns. The notification shall include the re-calculation of the particulate matter limits allowed by 40 CFR 63 Subpart MM.
[40 CFR 63.867(b)(3)(ii)]
 - c. A change in a continuous monitoring parameter, the value of a continuous monitoring parameter, or the range of values of a continuous monitoring parameter for the following process units: Nos. 2 and 3 Recovery Furnaces, Nos. 2 and 3 Smelt Dissolving Tanks, and Nos. 1 and 2 Lime Kilns.
[40 CFR 63.867(b)(3)(iii)]

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- d. An increase in the daily black liquor solids firing rate for the No. 2 Recovery Boiler or the No. 3 Recovery Boiler during any 24-hour averaging period by more than 10 percent above the level measured in the most recent performance test pursuant to 40 CFR 63 Subpart MM.
[40 CFR 63.867(b)(3)(iv)]
- 6.2.31 The Permittee shall develop and implement a written startup, shutdown and malfunction plan that describes in detail, procedures for operating and maintaining the source during periods of startup shutdown and malfunction and a program of corrective action for malfunctioning process and air pollution control equipment used to comply with 40 CFR 63 Subpart MM. In addition to the information required in 40 CFR 63.6(e), the plan must also include the requirements in 40 CFR 63.866(a)(1) and (2).
[40 CFR 63.866]
- 6.2.32 The Permittee shall implement the corrective action plan as developed in Condition 6.2.31 if any of the following monitoring exceedances occur:
- i. No. 2 Recovery Boiler opacity greater than 20% for 10 consecutive six-minute averages.
[40 CFR 63.864(k)(1)(i)]
 - ii. No. 3 Recovery Boiler opacity greater than 20% for 10 consecutive six-minute averages.
[40 CFR 63.864(k)(1)(i)]
 - iii. No. 1 Lime Kiln Scrubber differential pressure less than 7.5 inches of water while firing natural gas or less than 11.9 inches of water while firing fuel oil for any three-hour average.
[40 CFR 63.864(k)(1)(ii)]
 - iv. No. 1 Lime Kiln Scrubber flow less than 300 gpm for any three-hour average.
[40 CFR 63.864(k)(1)(ii)]
 - v. No. 2 Lime Kiln Scrubber differential pressure less than 23.4 inches of water for any three-hour average.
[40 CFR 63.864(k)(1)(ii)]
 - vi. No. 2 Lime Kiln Scrubber flow less than 540 gpm for any three-hour average.
[40 CFR 63.864(k)(1)(ii)]
 - vii. No. 2 Smelt Tank Scrubber flow less than 150-gpm for any three-hour average.
[40 CFR 63.864(k)(1)(ii)]
 - viii. No. 2 Smelt Tank Scrubber fan motor amperage reading less than 77 amps for any three-hour average.
[40 CFR 63.864(k)(1)(vi)]
 - ix. No. 3 Smelt Tank Scrubber flow less than 340-gpm for any three-hour average.

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[40 CFR 63.864(k)(1)(ii)]

- x. No. 3 Smelt Tank Scrubber fan motor amperage reading less than 68 amps for any three-hour average.

[40 CFR 63.864(k)(1)(vi)]

PART 7.0 OTHER SPECIFIC REQUIREMENTS

7.1 Operational Flexibility Associated with this Amendment

7.2 Off-Permit Changes Associated with this Amendment

7.3 Alternative Requirements Associated with this Amendment

[White Paper #2]

Not Applicable.

7.4 Insignificant Activities Associated with this Amendment

(see Attachment B for the list of Insignificant Activities in existence at the facility at the time of permit issuance)

7.5 Temporary Sources Associated with this Amendment

[391-3-1-.03(10)(d)5 and 40 CFR 70.6(e)]

Not Applicable.

7.6 Short-term Activities Associated with this Amendment

(see Section 4.40 of Permit application and White Paper #1)

Not Applicable.

7.7 Compliance Schedule/Progress Reports Associated with this Amendment

[391-3-1-.03(10)(d)3 and 40 CFR 70.6(c)(4)]

None applicable.

7.8 Emissions Trading Associated with this Amendment

[391-3-1-.03(10)(d)1(ii) and 40 CFR 70.6(a)(10)]

Not Applicable.

7.9 Acid Rain Requirements Associated with this Amendment

Not Applicable.

7.12 Revocation of Existing Permits and Amendments

The following Air Quality Permits and Amendments are subsumed by this permit and are hereby revoked:

Air Quality Permit Number(s)	Dates of Original Permit Issuance or Amendment
N/a	N/a

7.13 Pollution Prevention Associated with this Amendment

Not Applicable.

7.14 Specific Conditions Associated with this Amendment

None applicable.

PART 8.0 GENERAL PROVISIONS**8.23 Solvent Metal Cleaning**

- 8.23.1 Except as may be specified in other provisions of this Permit, the Permittee shall not cause, suffer, allow, or permit the operation of a cold cleaner degreaser unless the following requirements for control of emissions of the volatile organic compounds are satisfied: [391-3-1-.02(2)(ff)1]
- a. The degreaser shall be equipped with a cover to prevent escape of VOC during periods of non-use,
 - b. The degreaser shall be equipped with a device to drain cleaned parts before removal from the unit,
 - c. If the solvent volatility is 0.60 psi or greater measured at 100 °F, or if the solvent is heated above 120 °F, then one of the following control devices must be used:
 - i. The degreaser shall be equipped with a freeboard that gives a freeboard ratio of 0.7 or greater, or
 - ii. The degreaser shall be equipped with a water cover (solvent must be insoluble in and heavier than water), or
 - iii. The degreaser shall be equipped with a system of equivalent control, including but not limited to, a refrigerated chiller or carbon adsorption system.
 - d. Any solvent spray utilized by the degreaser must be in the form of a solid, fluid stream (not a fine, atomized or shower type spray) and at a pressure which will not cause excessive splashing, and
 - e. All waste solvent from the degreaser shall be stored in covered containers and shall not be disposed of by such a method as to allow excessive evaporation into the atmosphere.

8.24 Incinerators

- 8.24.1 Except as specified in the section dealing with conical burners, no person shall cause, let, suffer, permit, or allow the emissions of fly ash and/or other particulate matter from any incinerator, in amounts equal to or exceeding the following: [391-3-1-.02(2)(c)1-4]
- a. Units with charging rates of 500 pounds per hour or less of combustible waste, including water, shall not emit fly ash and/or particulate matter in quantities exceeding 1.0 pound per hour.
 - b. Units with charging rates in excess of 500 pounds per hour of combustible waste, including water, shall not emit fly ash and/or particulate matter in excess of 0.20 pounds per 100 pounds of charge.

- 8.24.2 No person shall cause, let, suffer, permit, or allow from any incinerator, visible emissions the opacity of which is equal to or greater than twenty (20) percent except for one six minute period per hour of not more than twenty-seven (27) percent opacity.
- 8.24.3 No person shall cause or allow particles to be emitted from an incinerator which are individually large enough to be visible to the unaided eye.
- 8.24.4 No person shall operate an existing incinerator unless:
 - a. It is a multiple chamber incinerator;
 - b. It is equipped with an auxiliary burner in the primary chamber for the purpose of creating a pre-ignition temperature of 800°F; and
 - c. It has a secondary burner to control smoke and/or odors and maintain a temperature of at least 1500°F in the secondary chamber.

8.25 Volatile Organic Liquid Handling and Storage

- 8.25.1 The Permittee shall ensure that each storage tank subject to the requirements of Rule 391-3-1-.02(2)(vv) “Volatile Organic Liquid Handling and Storage” is equipped with submerged fill pipes. For the purposes of this condition and the permit, a submerged fill pipe is defined as any fill pipe with a discharge opening which is within six inches of the tank bottom.
[391-3-1-.02(2)(vv)(1)]

8.26 Use of Any Credible Evidence or Information

- 8.26.1 Notwithstanding any other provisions of any applicable rule or regulation or requirement of this permit, for the purpose of submission of compliance certifications or establishing whether or not a person has violated or is in violation of any emissions limitation or standard, nothing in this permit or any Emission Limitation or Standard to which it pertains, shall preclude the use, including the exclusive use, of any credible evidence or information, relevant to whether a source would have been in compliance with applicable requirements if the appropriate performance or compliance test or procedure had been performed.
[391-3-1-.02(3)(a)]